ASAP (American Solar Action Plan)

ASAP

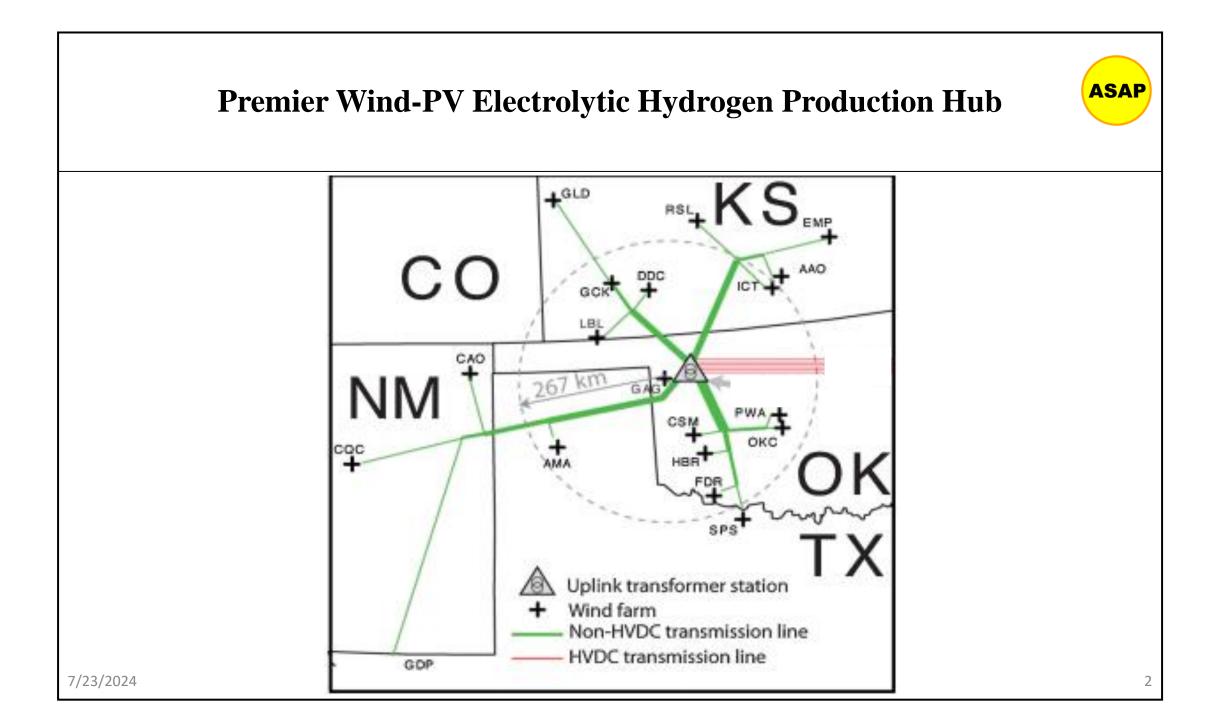
Panhandle Wind-PV Electrolytic Hydrogen System

July 2024 James Mason, Ph.D.

<u>ASAP</u>

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Panhandle Wind-PV Electrolytic Hydrogen System No Subsidies Are Included In This Analysis

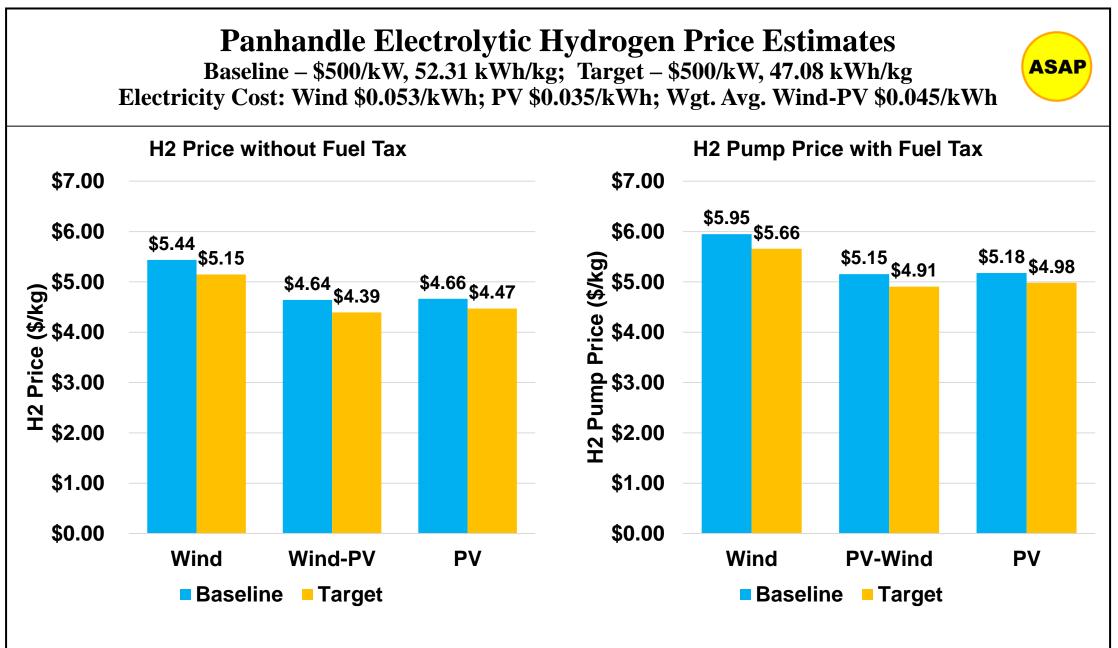
- Target Hydrogen Pump Price less than \$5.00/kg (including a \$0.51/kg State/Federal Fuel Tax)
- Annual Electrolyzer Purchase/Installation Capacity (GW_{dc el-in}) Schedule
 - 1 GW/Stage Development Stages 1-4 (1 GW Electrolyzer = 100,000 tpa H2)
 - 3 GW/Stage Development Stages 5-6 (Total Electrolyzer Capacity = 10 GW)
 - Delivered Cost of Wind and PV DC Electricity at \$0.035/kWh (Critical Maximum)

• Initial Hydrogen Markets (1 GW Electrolyzer New Capacity per Annum in Stages 1-4)

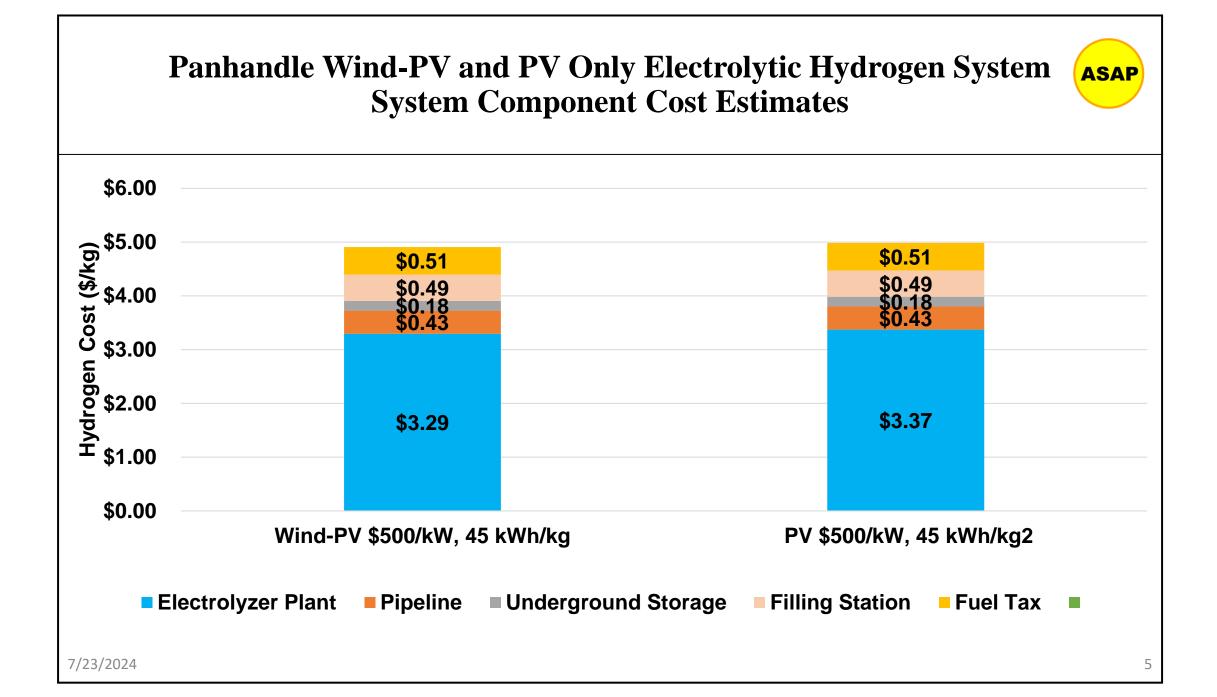
- 80% for Refinery/Ammonia/Fertilizer Plants with Pipeline Hydrogen Delivery
- 20% for Class 8 Fuel Cell Trucks with Fueling Centers with Pipeline Hydrogen Delivery
 - 6 Fueling Centers per Development Stage
 - Supports the Addition of 2,400 Class 8 Fuel Cell Trucks in Stages 1-4
- Hydrogen Pipelines
 - 600 Miles of Pipeline per Development Stage

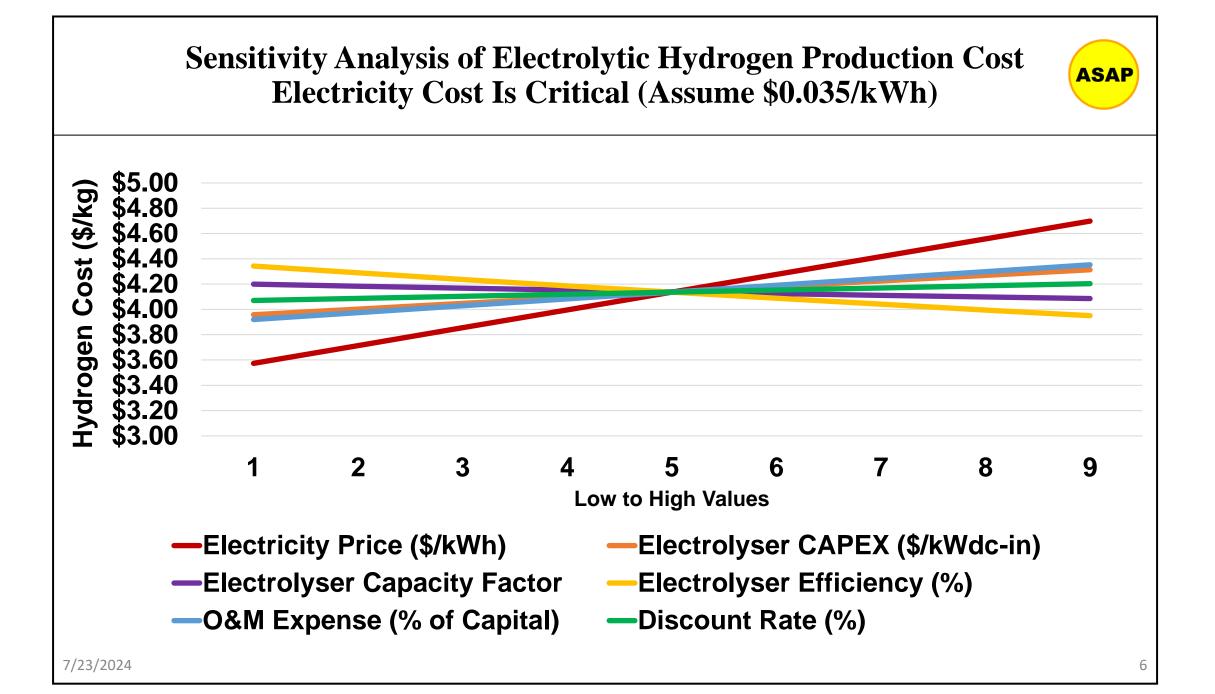
Hydrogen Underground Salt Storage Facilities

• 2 Salt Caverns – Each 45 Mcf with 8,000 t of Working Gas Storage at 1,700 psi (Working Gas 67% of Volume)



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Wind-PV Electrolysis Plant Development with Hydrogen Production Growth

	Electrolyzer (GW)	Wind (GW)	PV (GW)	Hydrogen Growth (Mtpa)
Stage 1	1.0	1.3	1.3	0.1
Stage 2	1.0	1.3	1.3	0.1
Stage 3	1.0	1.3	1.3	0.1
Stage 4	1.0	1.3	1.3	0.1
Stage 5	3.0	3.9	3.9	0.3
Stage 6	3.0	3.9	3.9	0.3
Total	10.0	13.0	13.0	1.0

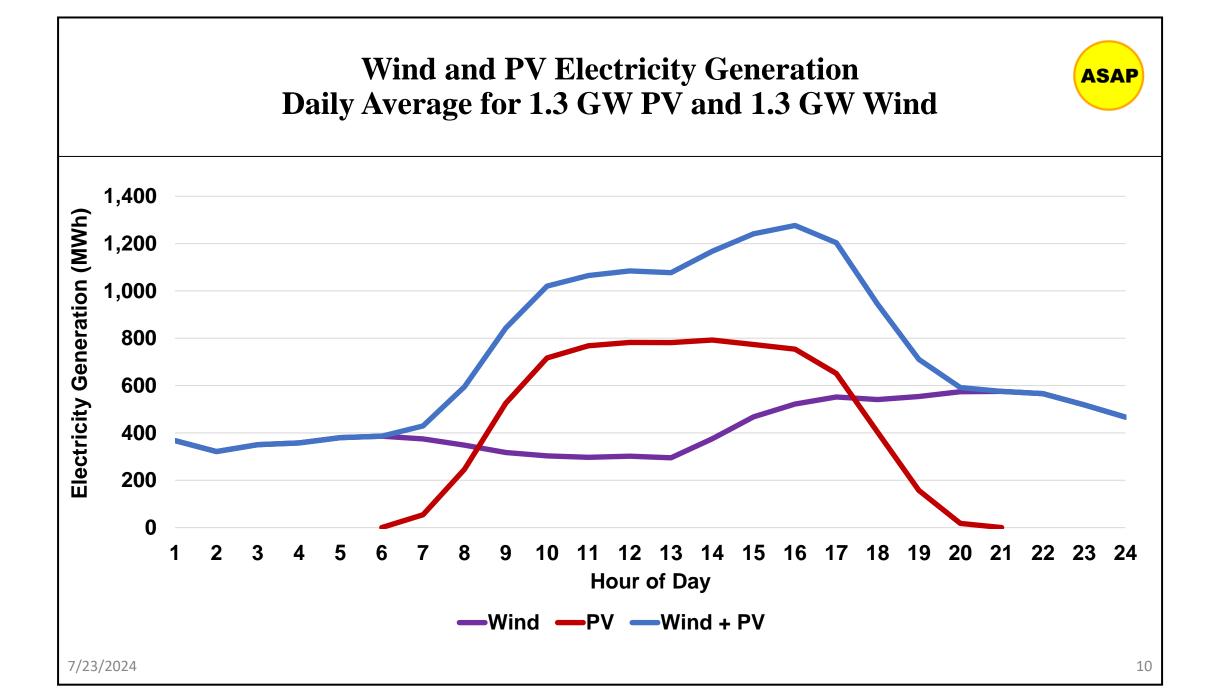
PV Electrolysis Plant Development with Hydrogen Production Growth

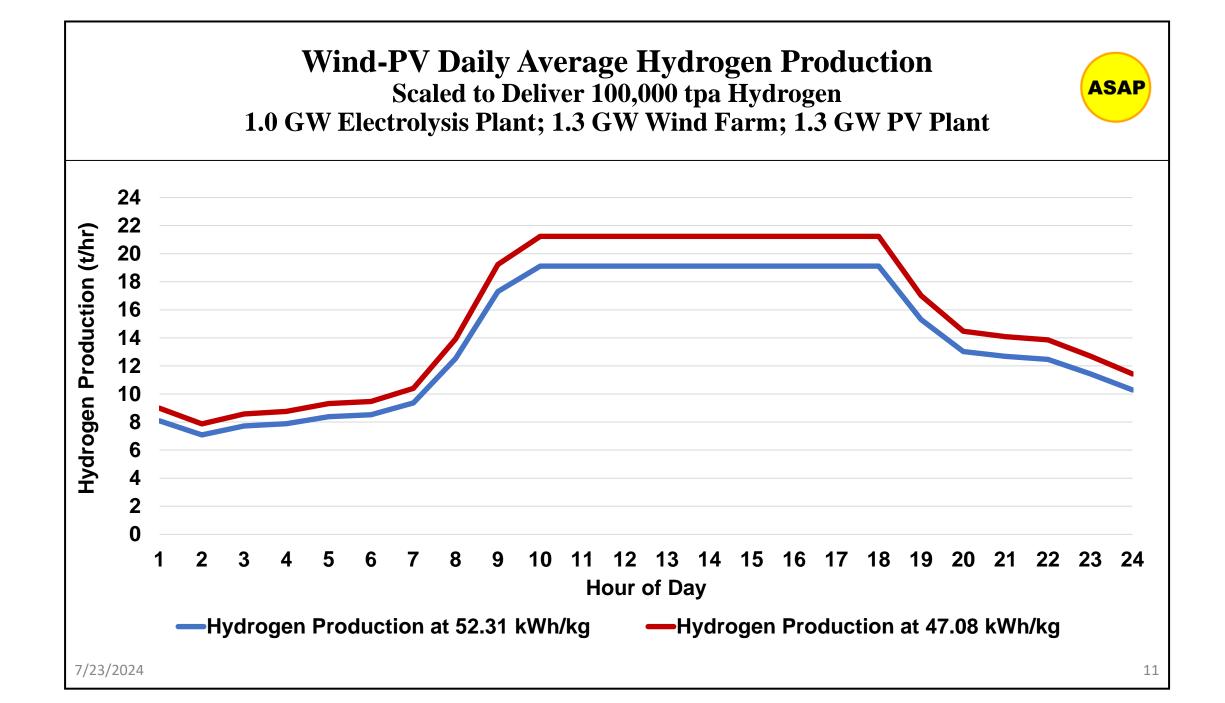
	Electrolyzer (GW)	PV (GW)	Hydrogen Growth (Mtpa)
Stage 1	1.6	2.8	0.1
Stage 2	1.6	2.8	0.1
Stage 3	1.6	2.8	0.1
Stage 4	1.6	2.8	0.1
Stage 5	4.8	8.4	0.3
Stage 6	4.8	8.4	0.3
Total	16.0	28.0	1.0

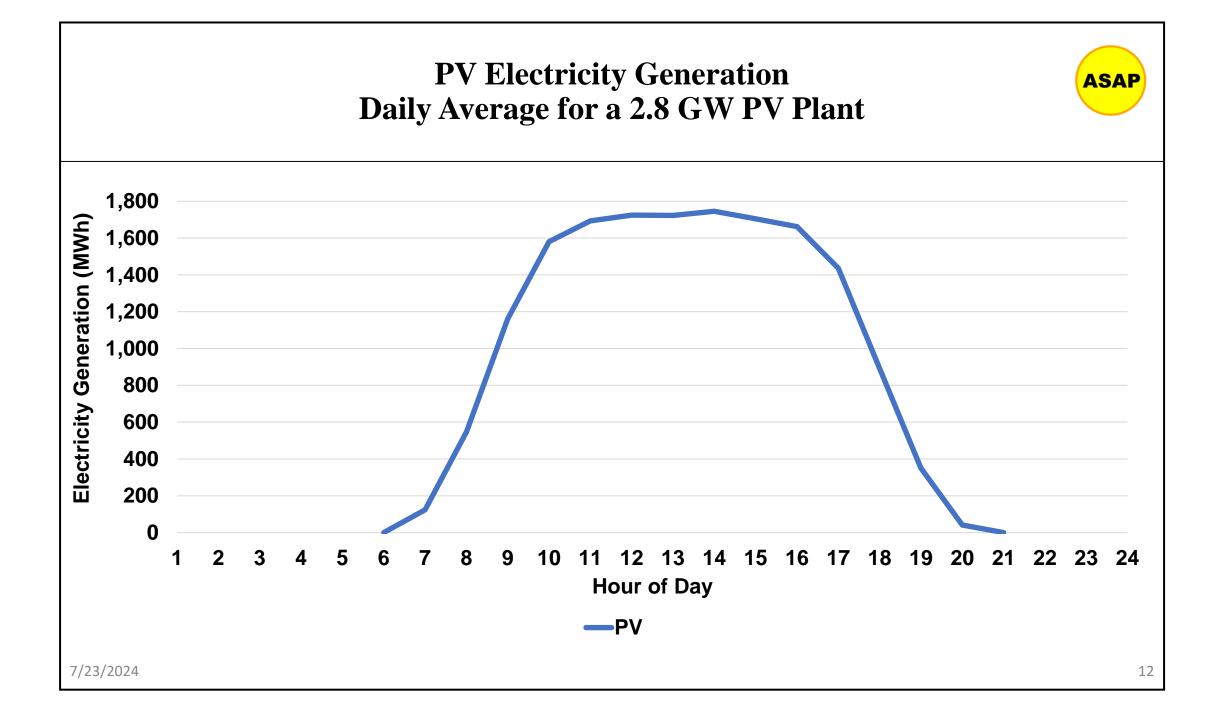


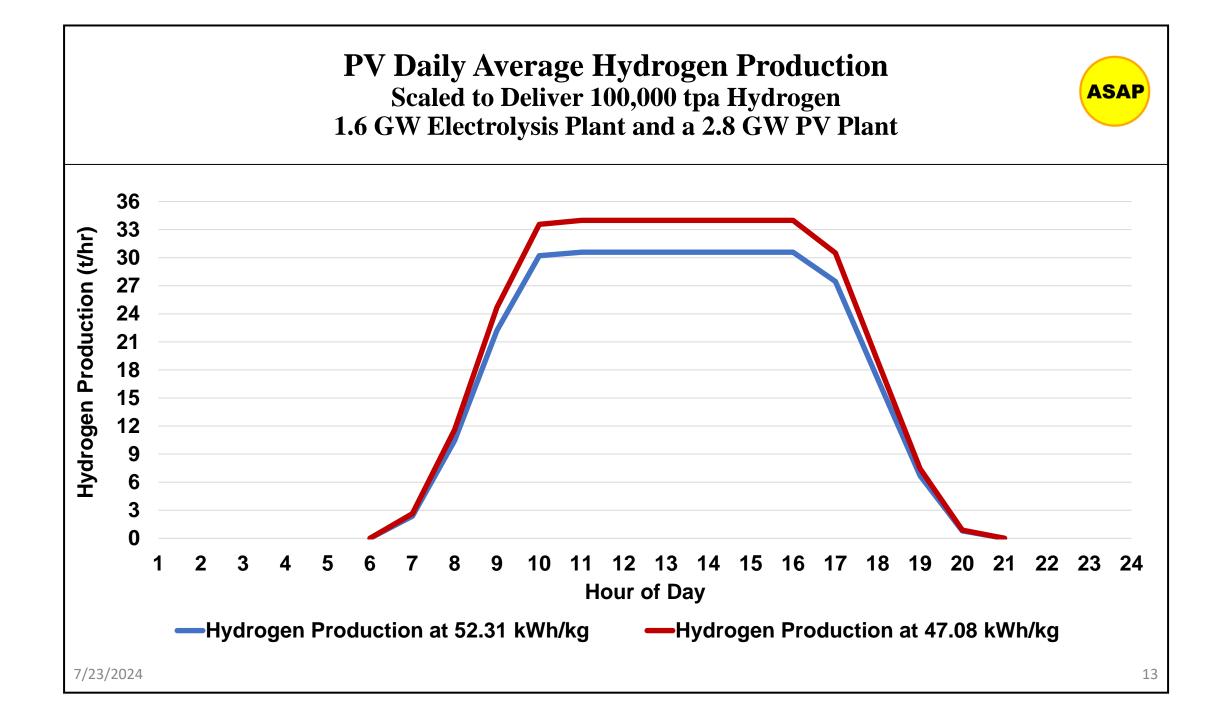
Wind and PV Electrolytic Hydrogen System Capacity Scaled for 100,000 tpa of Delivered Hydrogen

	Electrolyzer Capacity (MW)	PV Capacity (MW)	Wind Capacity (MW)	Hydrogen (Mtpa)
Wind	1,400	0	2,300	1.0
PV-Wind	1,000	1,300	1,300	1.0
PV	1,600	2,800	0	1.0









Wind and PV Electrolytic Hydrogen System CAPEX Scaled for 100,000 tpa of Delivered Hydrogen with a 50-Year Operating Life Electrolyzers \$500/kW_{dc-in} Wind Farm \$1,300/kW_{dc-out} PV Plant \$900/kW_{dc-out} 600 Mile Pipeline – \$180,000,000; Two Salt Storage Caverns – \$100,000,000; Six Heavy Freight Truck Fueling Stations – \$90,000,000

	Electrolysis Plant	PV Plant	Wind Farm 1st Gen	Wind Farm 2nd Gen	Downstream Components	Total CAPEX
Wind	\$700,000,000	\$0	\$2,990,000,000	\$1,196,000,000	\$373,600,000	\$5,259,600,000
PV-Wind	\$500,000,000	\$1,170,000,000	\$1,690,000,000	\$676,000,000	\$373,600,000	\$4,409,600,000
PV	\$800,000,000	\$2,520,000,000	\$0	\$0	\$373,600,000	\$3,693,600,000

CAPEX for Electrolysis Plant and Downstream Components Scaled for 100,000 tpa of Delivered Hydrogen

Capital Costs	Unit Cost	<u>Capex</u>
Electrolyzer Plant Total Installed Cost All Components (\$/kW _{dc el-in})	\$500	\$500,000,000
Electrolyzer Plant Land, Site Design, and Preparation Costs (\$/kW)	\$50	\$50,000,000
Pipeline 600 Miles (\$/mile)	\$3,000,000	
Pipeline Portion Allocated to 100,000 tpa H2 Plant	10%	\$180,000,000
Pipeline Compressor Stations Total Installed Cost (12 Stations – 50 mile)	\$1,500,000	
Pipeline Compressor Stations Portion Allocated to 100,000 tpa H2 Plant	10%	\$1,800,000
2 Underground 45-Mcf Salt Storage Caverns (\$/Cavern)	\$50,000,000	\$100,000,000
6 Fueling Stations (\$/Station)	\$15,000,000	\$90,000,000
Total Capex		\$923 million

Financial Assumptions



Discount Rate - Weighted Average Cost of Capital	
Discount Rate	10.1%
Annual Inflation	3.0%
Capital Recovery Period	20 Years
Capital Structure	
% Equity Capital	5.0%
% Debt Capital	95.0%
Cost of Capital	
Cost of Equity Capital	15.0%
Cost of Debt Capital	9.0%
Federal/State Income Tax Rate (Federal = 21%, Texas State Franchise Tax = 0.75%)	21.75%
CAPEX Depreciation	MACRS 20-yr
Replacement Costs Depreciation	MACRS 10-yr
7/23/2024	16

Electrolytic Hydrogen System Assumptions

Electrolyzer Annual Degradation Rate (%/annum)	1.0%
System Fugitive Hydrogen Loss Rate (%/annum)	3.0%
Compressors Powered by Grid Electricity (Grid Electricity Cost)	\$0.05/kWh
Pipeline Diameter to Deliver 1.0 Mta (diameter inches)	10.0
Pipeline Compressor Stations (Miles between Stations)	50
Underground Salt Storage 2 45-Mcf Sites (tonnes Working Gas H2 Storage at 1,700 psi)	16,000
Annual Hydrogen Storage Cycle (tonnes)	6,000-11,000
FC Class 8 Trucks Servicing San Antonio/Austin/Corpus Christi/Houston Freight Routes	2,400
Filling Station Pumps (# Pumps per Station – 2 Trucks/Hour for 10 Hours/Day)	20
Filling Station Truck Capacity/Station (# FC Class 8 Trucks)	400

Annual System Expense Estimates Scaled for 100,000 tpa of Delivered Hydrogn



Expenses	Unit Expense	Total Expense
Wind and PV Electricity Electrolysis Expense (\$/kWh)	\$0.035	\$192,500,000-\$173,300,000
Electrolyzer Efficiency (Avg kWh/kg H2)	52.31-47.08	
Electrolyzer Degradation (%/annum with Rebuild Year 10)	1.0%	
Electrolysis Plant O&M (% Capex)	3.0%	\$15,000,000
Pipeline O&M Expense (% Capex)	2.0%	\$3,600,000
Compression Station O&M Expense 12 Stations (% Capex)	4.0%	\$720,000
Underground Storage O&M Expense (% Capex)	2.0%	\$2,000,000
Filling Station O&M Expense 6 Stations (% Capex)	25.0%	\$18,000,000
Insurance Expense (% Capex)	0.5%	\$4,618,000
Compression Electricity Expense (\$/kWh)	\$0.050	\$17,016,237
Water Expense Desalinated (\$/1000 gallons)	\$10.00	\$3,132,417
Total Expenses		\$279,000,000-\$260,000,000

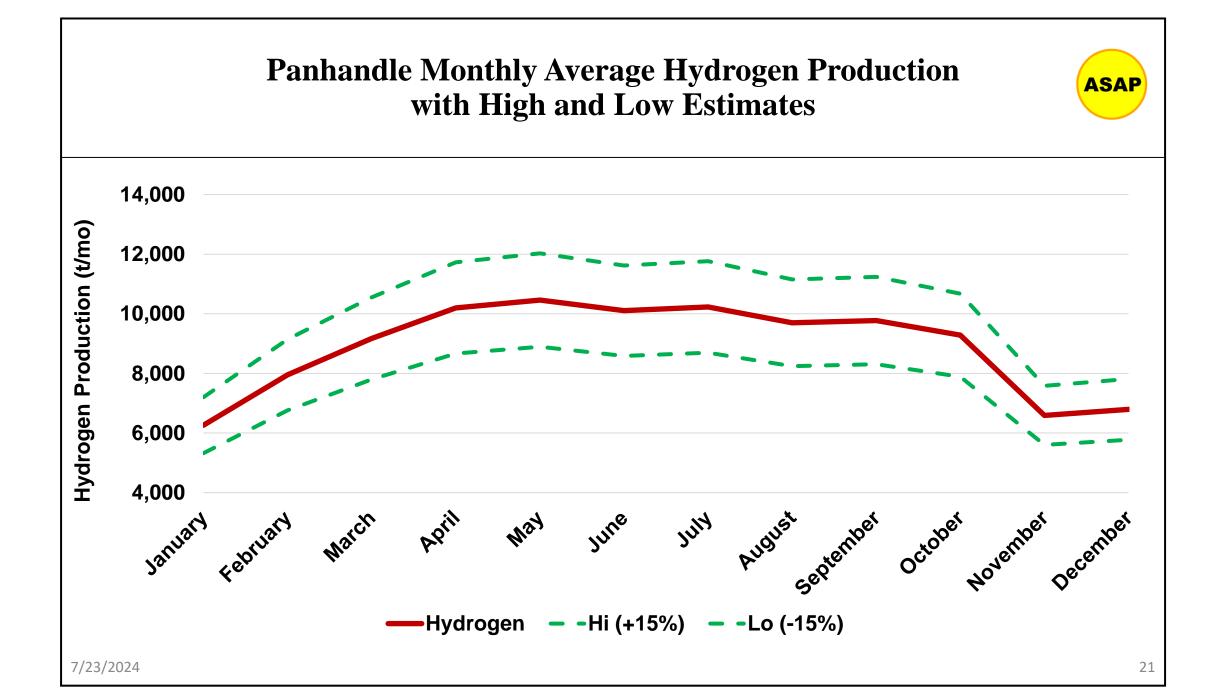
Hydrogen System Water Consumption and Expense Gulf Coast Desalination Plant and Pipeline Water Delivery Delivered Water Cost - \$10.00/1000 gallons (\$0.010/gal)



Water Cost (\$/gal)	\$0.01200	
	Quantity (gal)	Water Expense
H2 Electrolyzer Water Expense (11.13 liters water/kg H2)	303,117,004	\$3,031,170
Electrolyzer Cooling Water Expense (300 liters water/kg H2)	7,461,449	\$74,614
Pipeline Compressor Cooling Water Expense (50 liters water/kg H2)	1,243,575	\$12,436
Storage Compressor Cooling Water Expense (50 liters water/kg H2)	146,762	\$1,761
Filling Station Compressor Cooling Water Expense (50 liters water/kg H2)	1,243,575	\$12,436
Total Water Consumption and Expense	313,213,002	\$3,132,417

Hydrogen Compression Energy Estimates Grid Electricity Expense

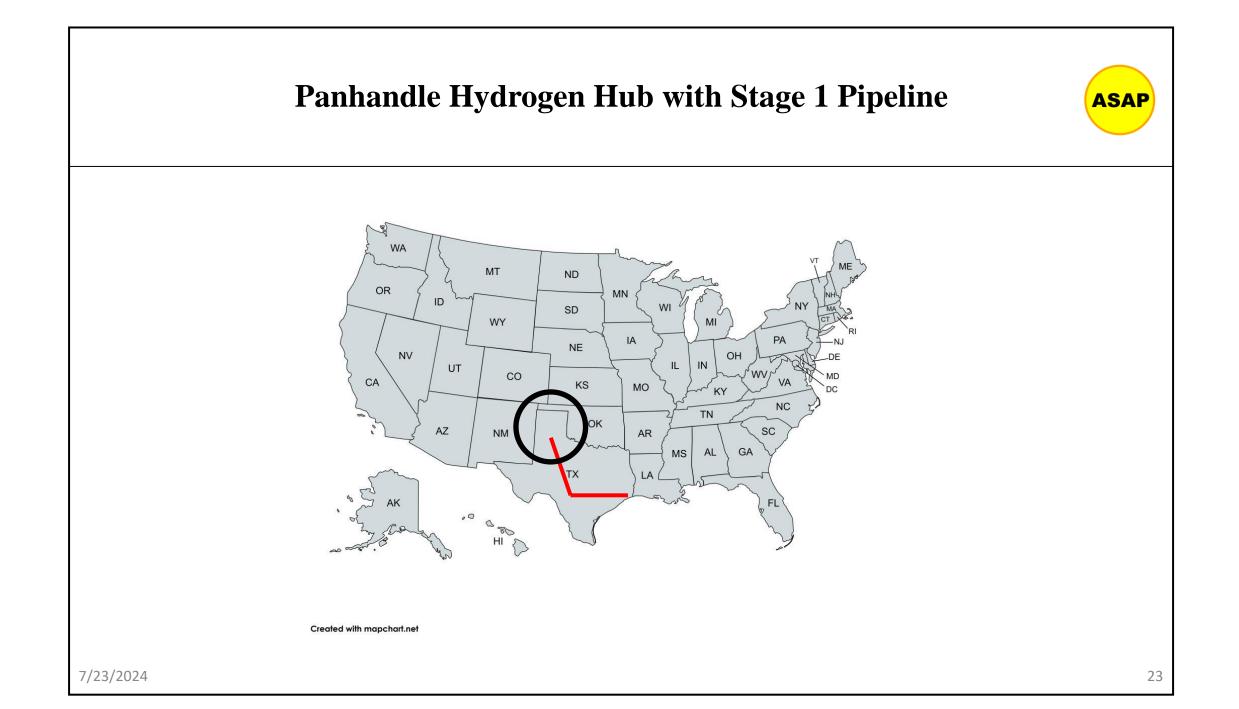
Grid Electricity Cost (\$/kWh)	\$0.050				
	Quantity	Pressure (Begin and End)	Energy		Electricity Expense
Electrolyzer Plant to Pipeline	103,093 tpa	290-1000 psi	0.770	kWh/kg	\$3,969,081
Compressor Stations (12)	103,093 tpa	700-1000 psi	0.130	kWh/kg	\$8,041,254
Filling Stations (6)	100,000 tpa	900-12760 psi	1.757	kWh/kg	\$9,056,720
Underground Storage (2)	10,000 tpa	900-1700 psi	0.38	kWh/kg	\$190,000
Total Electricity Expense					\$21,257,055



Hydrogen Storage Estimates Assume a Constant 8,333 tpm of Delivered Hydrogen



Tonnes	Production			Storage		
	Average	Hi (+15%)	Lo (-15%)	Average	e Hi (+15%)	Lo (-15%)
January	6,318	7,265	5,370	2,015	1,068	2,963
February	7,978	9,175	6,781	355	0	1,552
March	9,213	10,595	7,831	C	0	502
April	10,233	11,768	8,698	(0	0
Мау	10,526	12,105	8,947	C	0	0
June	10,168	11,693	8,643	C	0	0
July	10,292	11,836	8,748	C	0	0
August	9,718	11,176	8,260	(0	73
September	9,792	11,260	8,323	C	0	10
October	9,313	10,710	7,916	C	0	417
November	6,598	7,588	5,609	1,735	745	2,724
December	6,794	7,814	5,775	1,539	519	2,558
Total (<mark>Storage</mark>)	106,943	122,984	90,901	<mark>5,644</mark>	2,332	<mark>10,798</mark>



Panhandle Hydrogen Hub with Southern Pipeline Network Upon Stage 6 Completion

