# ASAP (American Solar Action Plan)

ASAP

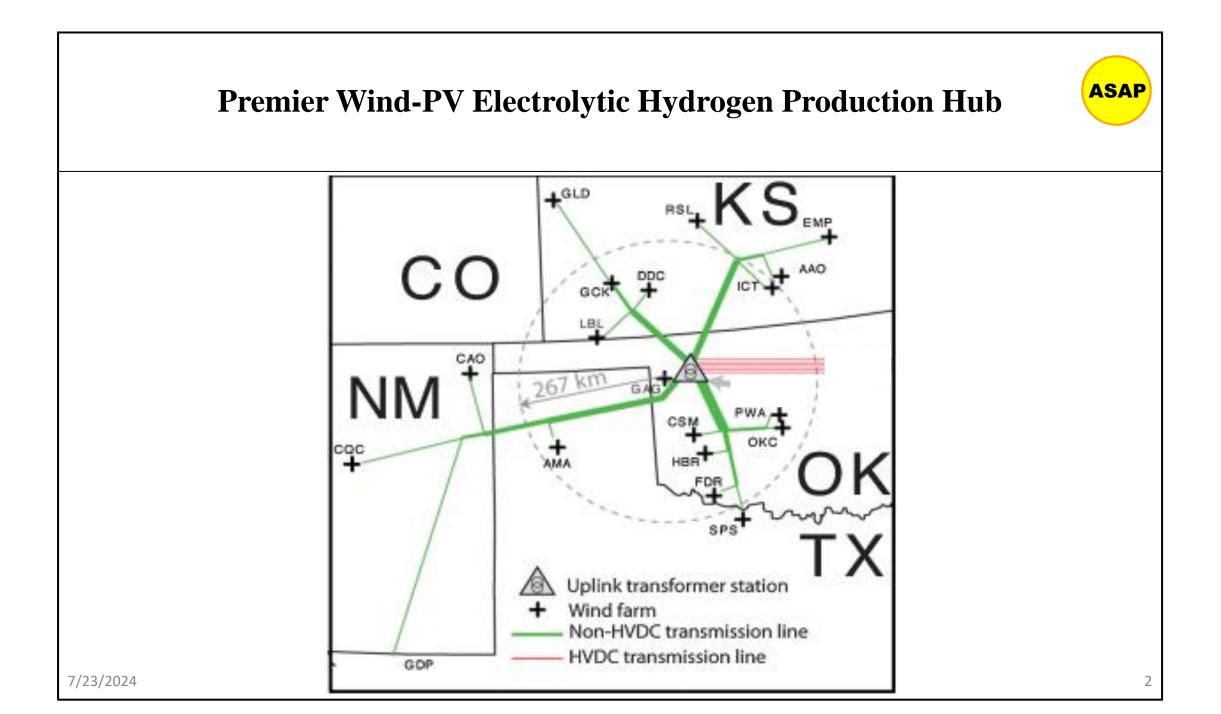
# Panhandle Wind-PV Electrolytic Hydrogen System

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<u>ASAP</u>

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7/23/2024



### Panhandle Wind-PV Electrolytic Hydrogen System No Subsidies Are Included In This Analysis

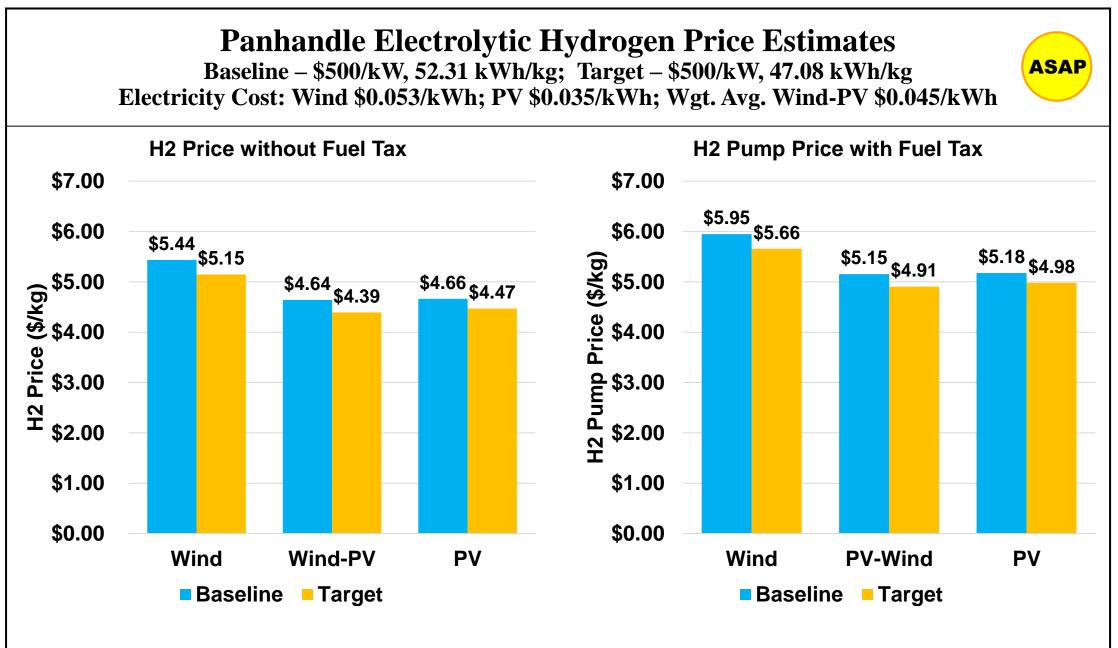
- Target Hydrogen Pump Price less than \$5.00/kg (including a \$0.51/kg State/Federal Fuel Tax)
- Annual Electrolyzer Purchase/Installation Capacity (GW<sub>dc el-in</sub>) Schedule
  - 1 GW/Stage Development Stages 1-4 (1 GW Electrolyzer = 100,000 tpa H2)
  - 3 GW/Stage Development Stages 5-6 (Total Electrolyzer Capacity = 10 GW)
  - Delivered Cost of Wind and PV DC Electricity at \$0.035/kWh (Critical Maximum)

#### • Initial Hydrogen Markets (1 GW Electrolyzer New Capacity per Annum in Stages 1-4)

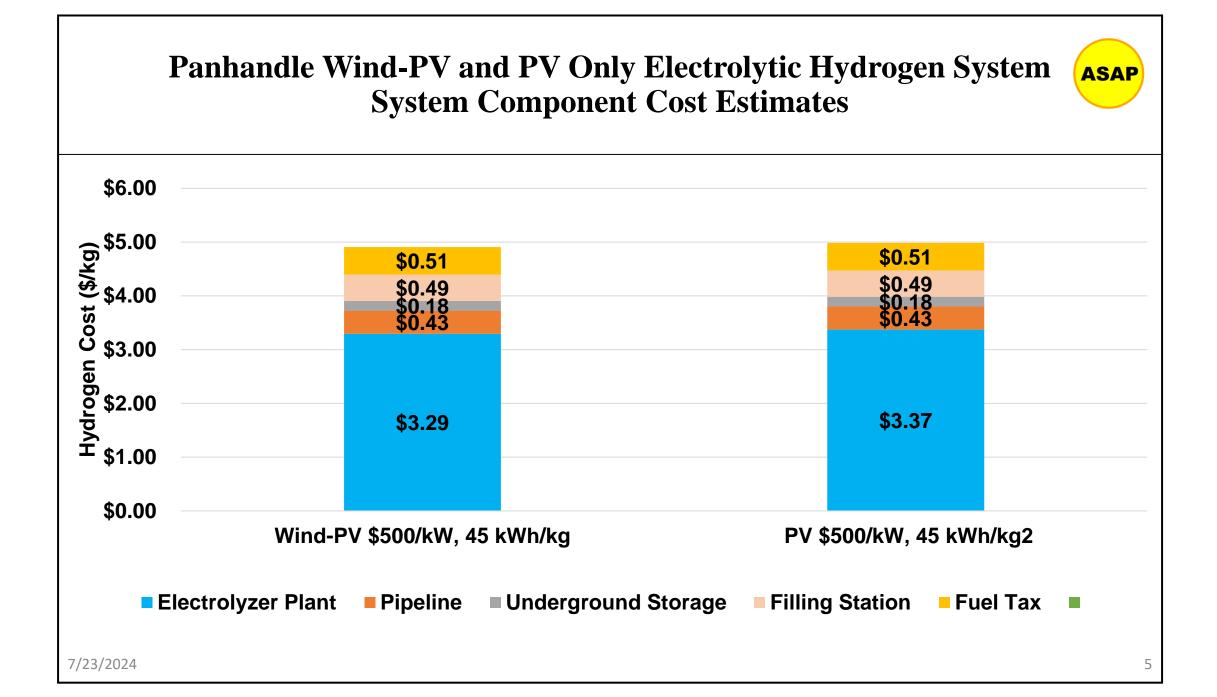
- 80% for Refinery/Ammonia/Fertilizer Plants with Pipeline Hydrogen Delivery
- 20% for Class 8 Fuel Cell Trucks with Fueling Centers with Pipeline Hydrogen Delivery
  - 6 Fueling Centers per Development Stage
  - Supports the Addition of 2,400 Class 8 Fuel Cell Trucks in Stages 1-4
- Hydrogen Pipelines
  - 600 Miles of Pipeline per Development Stage

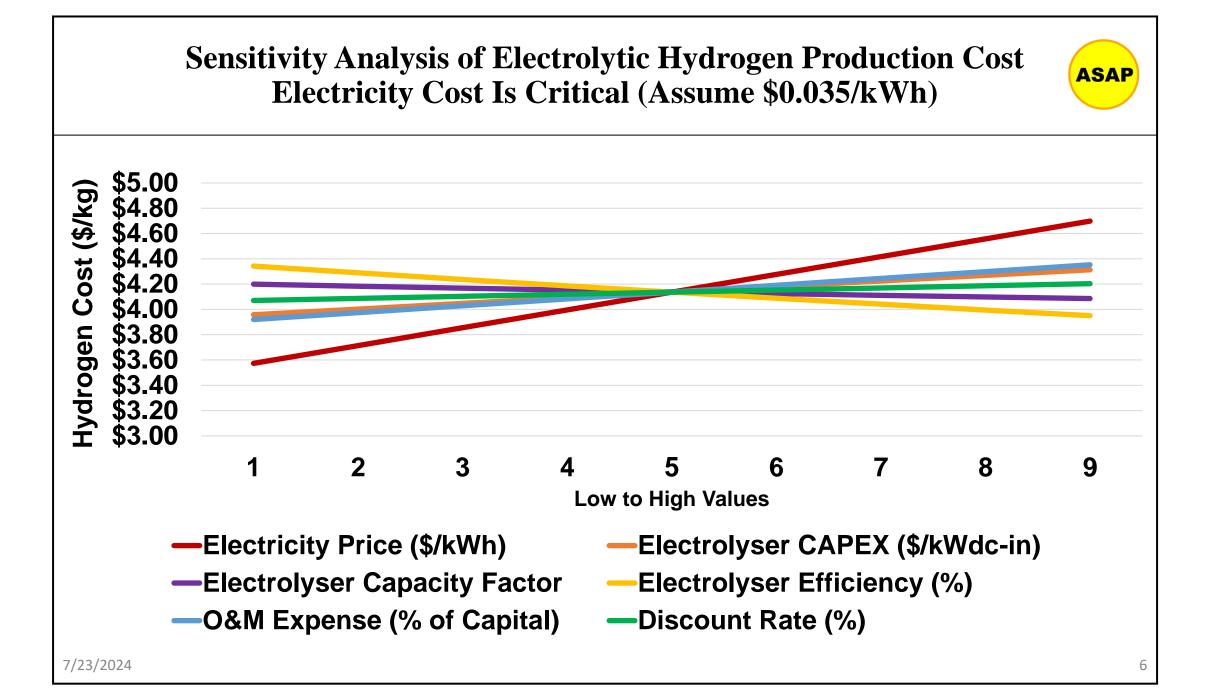
#### Hydrogen Underground Salt Storage Facilities

• 2 Salt Caverns – Each 45 Mcf with 8,000 t of Working Gas Storage at 1,700 psi (Working Gas 67% of Volume)



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### Wind-PV Electrolysis Plant Development with Hydrogen Production Growth

	Electrolyzer (GW)	Wind (GW)	PV (GW)	Hydrogen Growth (Mtpa)
Stage 1	1.0	1.3	1.3	0.1
Stage 2	1.0	1.3	1.3	0.1
Stage 3	1.0	1.3	1.3	0.1
Stage 4	1.0	1.3	1.3	0.1
Stage 5	3.0	3.9	3.9	0.3
Stage 6	3.0	3.9	3.9	0.3
Total	10.0	13.0	13.0	1.0

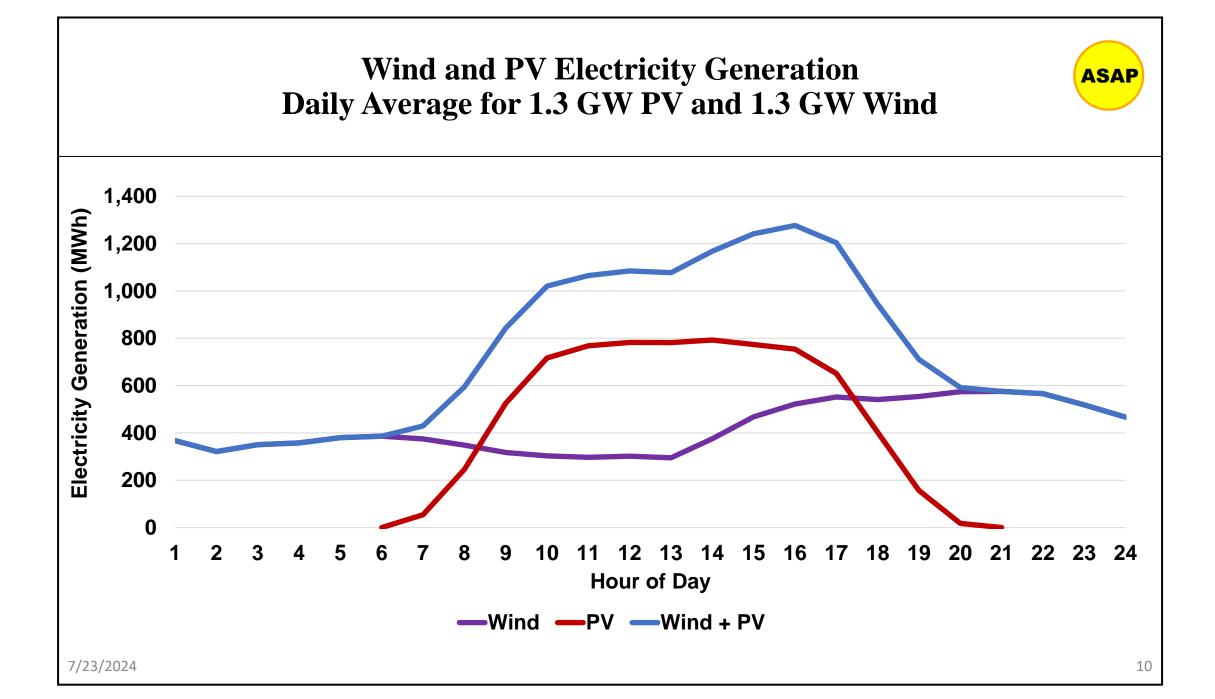
# **PV Electrolysis Plant Development** with Hydrogen Production Growth

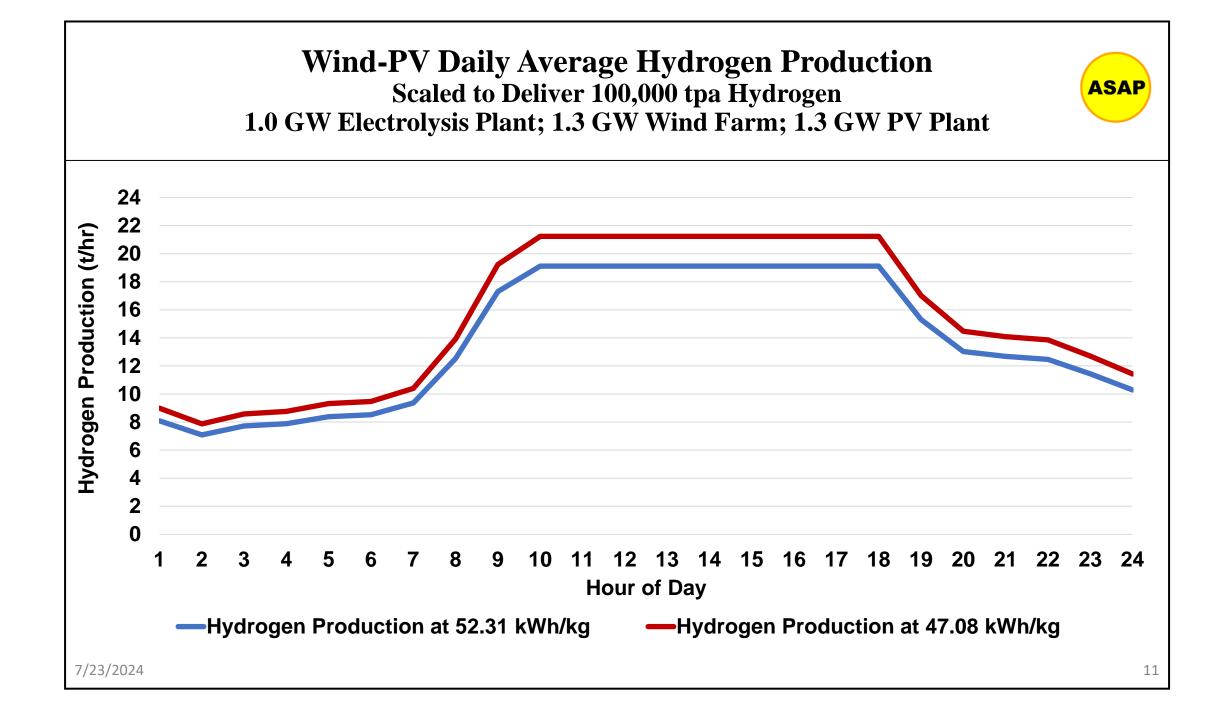
	Electrolyzer (GW)	PV (GW)	Hydrogen Growth (Mtpa)
Stage 1	1.6	2.8	0.1
Stage 2	1.6	2.8	0.1
Stage 3	1.6	2.8	0.1
Stage 4	1.6	2.8	0.1
Stage 5	4.8	8.4	0.3
Stage 6	4.8	8.4	0.3
Total	16.0	28.0	1.0

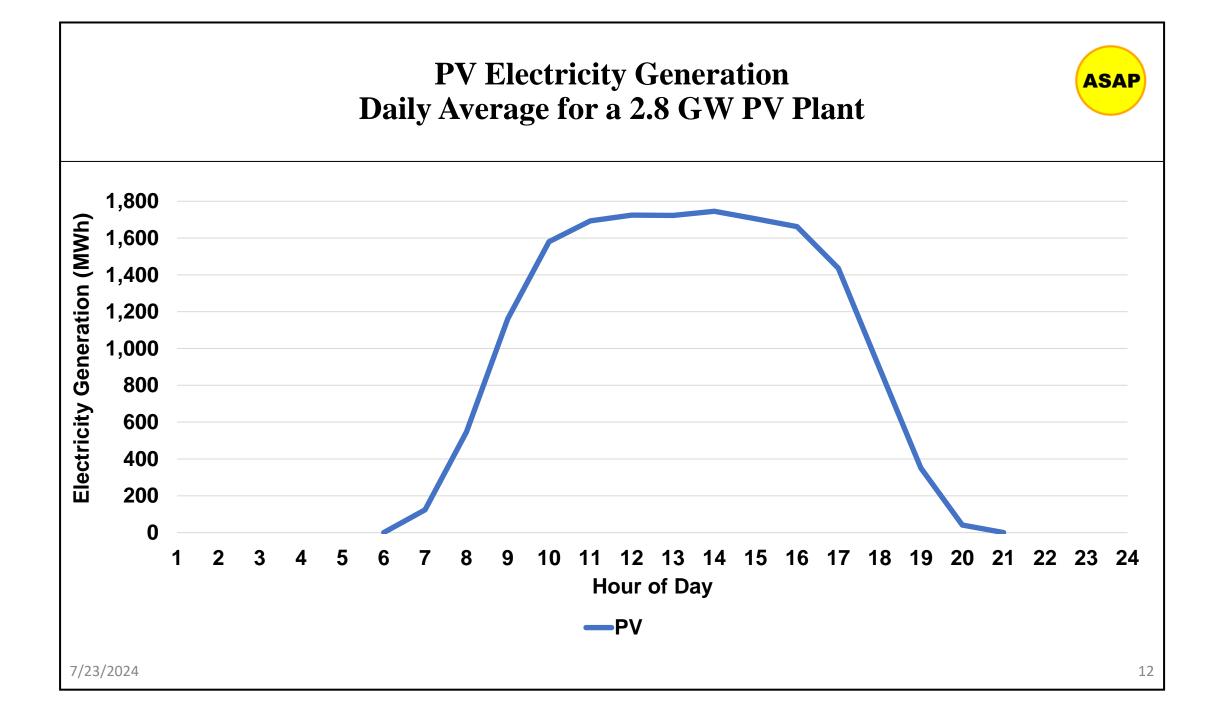


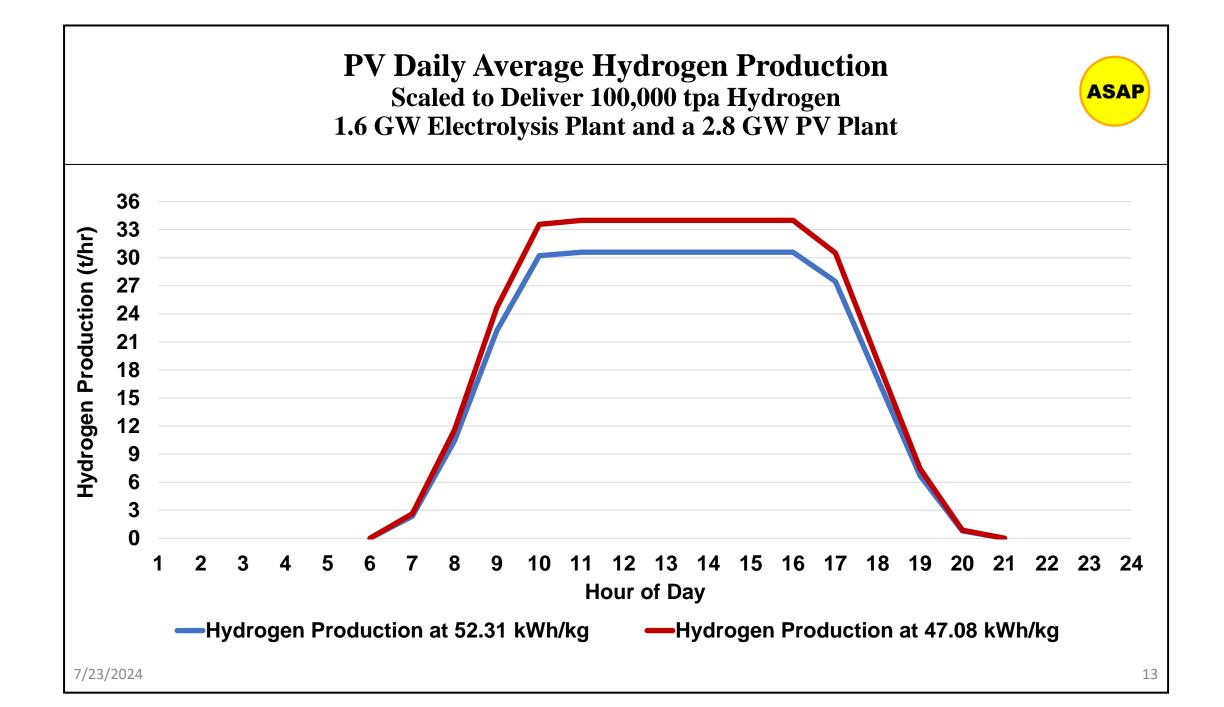
#### Wind and PV Electrolytic Hydrogen System Capacity Scaled for 100,000 tpa of Delivered Hydrogen

	Electrolyzer Capacity (MW)	PV Capacity (MW)	Wind Capacity (MW)	Hydrogen (Mtpa)
Wind	1,400	0	2,300	1.0
PV-Wind	1,000	1,300	1,300	1.0
PV	1,600	2,800	0	1.0









Wind and PV Electrolytic Hydrogen System CAPEX Scaled for 100,000 tpa of Delivered Hydrogen with a 50-Year Operating Life Electrolyzers \$500/kW<sub>dc-in</sub> Wind Farm \$1,300/kW<sub>dc-out</sub> PV Plant \$900/kW<sub>dc-out</sub> 600 Mile Pipeline – \$180,000,000; Two Salt Storage Caverns – \$100,000,000; Six Heavy Freight Truck Fueling Stations – \$90,000,000

	Electrolysis Plant	PV Plant	Wind Farm 1st Gen	Wind Farm 2nd Gen	Downstream Components	Total CAPEX
Wind	\$700,000,000	\$0	\$2,990,000,000	\$1,196,000,000	\$373,600,000	\$5,259,600,000
<b>PV-Wind</b>	\$500,000,000	\$1,170,000,000	\$1,690,000,000	\$676,000,000	\$373,600,000	\$4,409,600,000
PV	\$800,000,000	\$2,520,000,000	\$0	\$0	\$373,600,000	\$3,693,600,000

#### CAPEX for Electrolysis Plant and Downstream Components Scaled for 100,000 tpa of Delivered Hydrogen

Capital Costs	Unit Cost	<u>Capex</u>
Electrolyzer Plant Total Installed Cost All Components (\$/kW <sub>dc el-in</sub> )	\$500	\$500,000,000
Electrolyzer Plant Land, Site Design, and Preparation Costs (\$/kW)	\$50	\$50,000,000
Pipeline 600 Miles (\$/mile)	\$3,000,000	
Pipeline Portion Allocated to 100,000 tpa H2 Plant	10%	\$180,000,000
Pipeline Compressor Stations Total Installed Cost (12 Stations – 50 mile)	\$1,500,000	
Pipeline Compressor Stations Portion Allocated to 100,000 tpa H2 Plant	10%	\$1,800,000
2 Underground 45-Mcf Salt Storage Caverns (\$/Cavern)	\$50,000,000	\$100,000,000
6 Fueling Stations (\$/Station)	\$15,000,000	\$90,000,000
Total Capex		\$923 million

# **Financial Assumptions**



Discount Rate - Weighted Average Cost of Capital	
Discount Rate	10.1%
Annual Inflation	3.0%
Capital Recovery Period	20 Years
Capital Structure	
% Equity Capital	5.0%
% Debt Capital	95.0%
Cost of Capital	
Cost of Equity Capital	15.0%
Cost of Debt Capital	9.0%
Federal/State Income Tax Rate (Federal = 21%, Texas State Franchise Tax = 0.75%)	21.75%
CAPEX Depreciation	MACRS 20-yr
Replacement Costs Depreciation	MACRS 10-yr
7/23/2024	16

# **Electrolytic Hydrogen System Assumptions**

Electrolyzer Annual Degradation Rate (%/annum)	1.0%
System Fugitive Hydrogen Loss Rate (%/annum)	3.0%
Compressors Powered by Grid Electricity (Grid Electricity Cost)	\$0.05/kWh
Pipeline Diameter to Deliver 1.0 Mta (diameter inches)	10.0
Pipeline Compressor Stations (Miles between Stations)	50
Underground Salt Storage 2 45-Mcf Sites (tonnes Working Gas H2 Storage at 1,700 psi)	16,000
Annual Hydrogen Storage Cycle (tonnes)	6,000-11,000
FC Class 8 Trucks Servicing San Antonio/Austin/Corpus Christi/Houston Freight Routes	2,400
Filling Station Pumps (# Pumps per Station – 2 Trucks/Hour for 10 Hours/Day)	20
Filling Station Truck Capacity/Station (# FC Class 8 Trucks)	400

#### Annual System Expense Estimates Scaled for 100,000 tpa of Delivered Hydrogn



Expenses	Unit Expense	Total Expense
Wind and PV Electricity Electrolysis Expense (\$/kWh)	\$0.035	\$192,500,000-\$173,300,000
Electrolyzer Efficiency (Avg kWh/kg H2)	52.31-47.08	
Electrolyzer Degradation (%/annum with Rebuild Year 10)	1.0%	
Electrolysis Plant O&M (% Capex)	3.0%	\$15,000,000
Pipeline O&M Expense (% Capex)	2.0%	\$3,600,000
Compression Station O&M Expense 12 Stations (% Capex)	4.0%	\$720,000
Underground Storage O&M Expense (% Capex)	2.0%	\$2,000,000
Filling Station O&M Expense 6 Stations (% Capex)	25.0%	\$18,000,000
Insurance Expense (% Capex)	0.5%	\$4,618,000
Compression Electricity Expense (\$/kWh)	\$0.050	\$17,016,237
Water Expense Desalinated (\$/1000 gallons)	\$10.00	\$3,132,417
Total Expenses		\$279,000,000-\$260,000,000

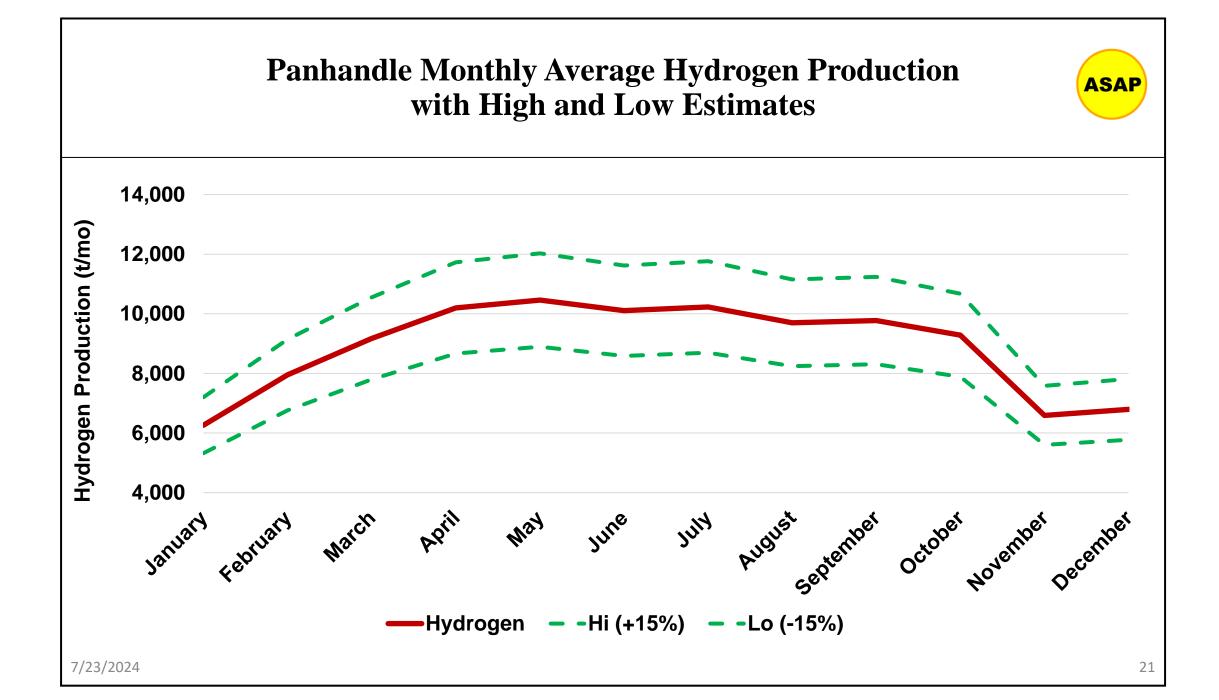
#### Hydrogen System Water Consumption and Expense Gulf Coast Desalination Plant and Pipeline Water Delivery Delivered Water Cost - \$10.00/1000 gallons (\$0.010/gal)



Water Cost (\$/gal)	\$0.01200	
	Quantity (gal)	Water Expense
H2 Electrolyzer Water Expense (11.13 liters water/kg H2)	303,117,004	\$3,031,170
Electrolyzer Cooling Water Expense (300 liters water/kg H2)	7,461,449	\$74,614
Pipeline Compressor Cooling Water Expense (50 liters water/kg H2)	1,243,575	\$12,436
Storage Compressor Cooling Water Expense (50 liters water/kg H2)	146,762	\$1,761
Filling Station Compressor Cooling Water Expense (50 liters water/kg H2)	1,243,575	\$12,436
Total Water Consumption and Expense	313,213,002	\$3,132,417

### Hydrogen Compression Energy Estimates Grid Electricity Expense

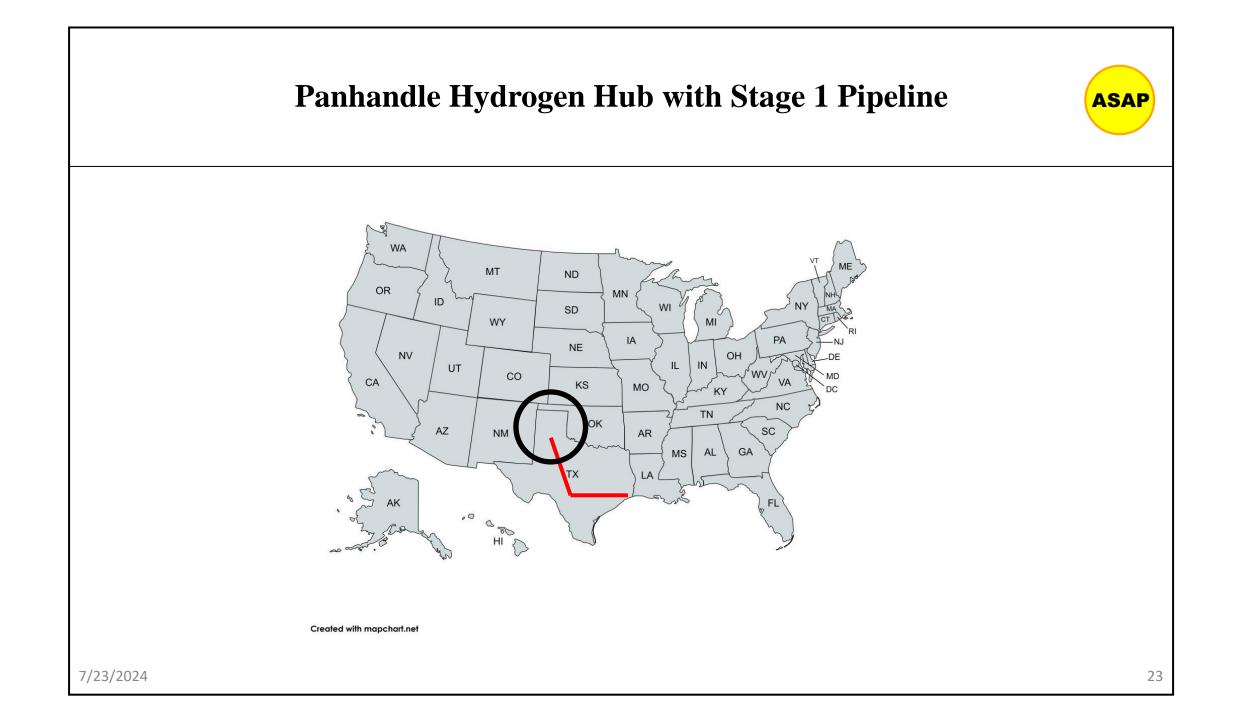
Grid Electricity Cost (\$/kWh)	\$0.050				
	Quantity	Pressure (Begin and End)	Energy		Electricity Expense
Electrolyzer Plant to Pipeline	103,093 tpa	290-1000 psi	0.770	kWh/kg	\$3,969,081
Compressor Stations (12)	103,093 tpa	700-1000 psi	0.130	kWh/kg	\$8,041,254
Filling Stations (6)	100,000 tpa	900-12760 psi	1.757	kWh/kg	\$9,056,720
Underground Storage (2)	10,000 tpa	900-1700 psi	0.38	kWh/kg	\$190,000
Total Electricity Expense					\$21,257,055



### Hydrogen Storage Estimates Assume a Constant 8,333 tpm of Delivered Hydrogen



Tonnes	<b>Production</b>			Storage		
	Average	Hi (+15%)	Lo (-15%)	Average	e Hi (+15%)	Lo (-15%)
January	6,318	7,265	5,370	2,015	1,068	2,963
February	7,978	9,175	6,781	355	0	1,552
March	9,213	10,595	7,831	C	0	502
April	10,233	11,768	8,698	(	0	0
Мау	10,526	12,105	8,947	C	0	0
June	10,168	11,693	8,643	C	0	0
July	10,292	11,836	8,748	C	0	0
August	9,718	11,176	8,260	(	0	73
September	9,792	11,260	8,323	C	0	10
October	9,313	10,710	7,916	C	0	417
November	6,598	7,588	5,609	1,735	745	2,724
December	6,794	7,814	5,775	1,539	519	2,558
Total ( <mark>Storage</mark> )	106,943	122,984	90,901	<mark>5,644</mark>	2,332	<mark>10,798</mark>



### Panhandle Hydrogen Hub with Southern Pipeline Network Upon Stage 6 Completion

